



Yale-NUIST Center on Atmospheric Environment



A discussion on the paper “Particle Loss Calculator – a new software tool for the assessment of the performance of aerosol inlet systems”

By S.-L. von der Weiden et al.

Atmospheric Measurement Techniques

IF: 3.206

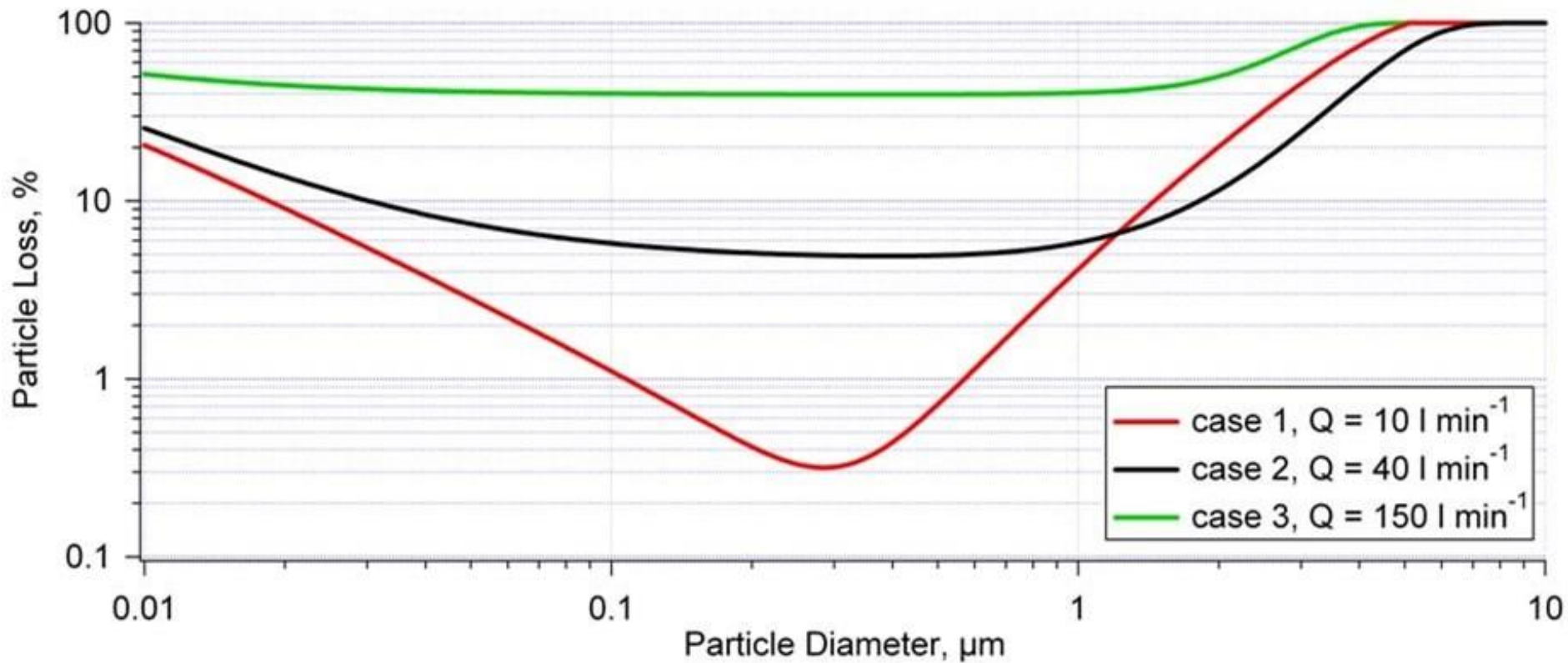
Liu Xiaoyan
2014-09-19

Outline

- Introduction
- Theory and method
- Operation
- Validation measurements
- Applications
- Summary

Introduction

- For aerosol measurement instruments, there's always an inlet system to transport aerosols from a sampling location to the analyser through some length of tubing, where aerosol particle loss due to a number of mechanisms exists.
- The inlet system with better performance is the one with less particle loss and higher sampling efficiency.
- Particle Loss Calculator(PLC) is a software which produces graphs showing particle loss on Y-axis and particle size on X-axis after inputting parameters of the inlet system.



$$d_a = d_{phys} \left(\frac{\rho_p}{\rho_0} \right)^{1/2}$$

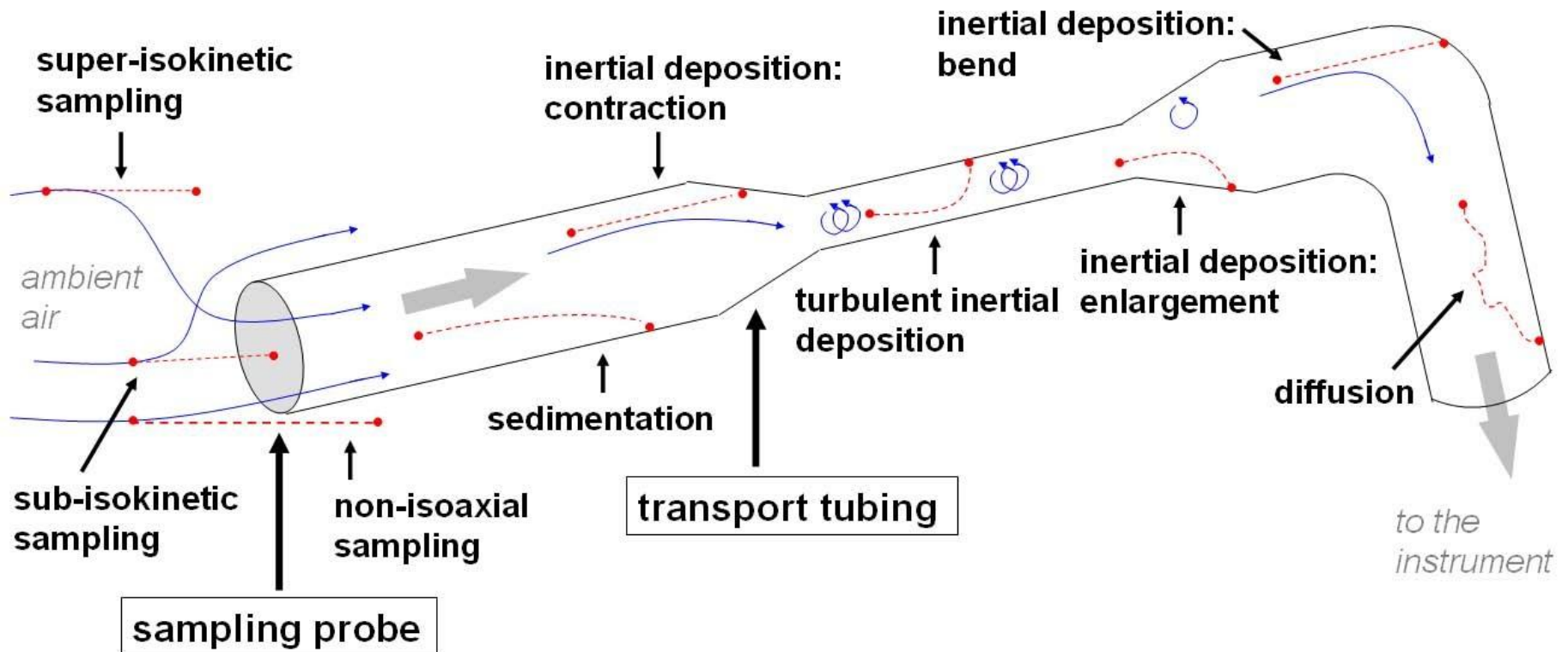
d_{phys} physical diameter

ρ_p density of the particles

ρ_0 standard density of 1g/cm^3 (Willeke and Baron, 2005)

Theory and method

● Particle loss mechanisms



Also include electrostatic deposition, thermophoreses, diffusiophoresis, interception and coagulation.

Theory and method

- Overall efficiency η_{inlet}

The ratio of the number concentration of particles behind the tube and the number concentration of particles in front of it.

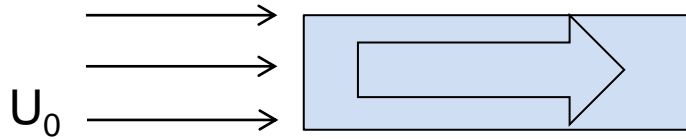
$$\eta_{inlet}(d_a) = \eta_{sampling}(d_a) \cdot \eta_{transport}(d_a)$$

(Willeke and Baron, 2005)

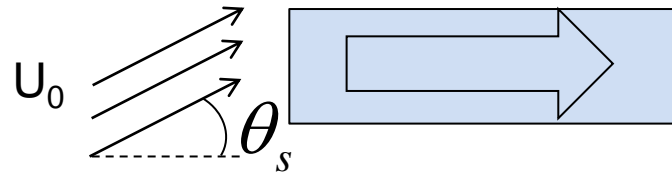
Theory and method

- Sampling situations:

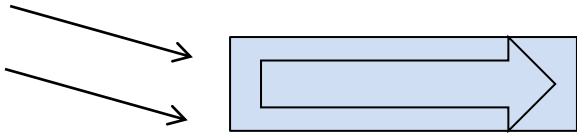
- Isoaxial sampling



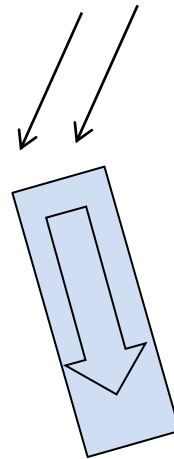
- Non-isoaxial sampling



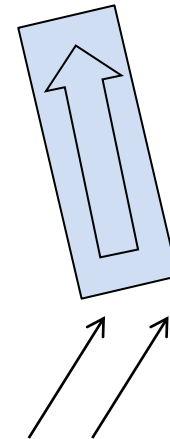
- Non-isaxial sampling



I_w : Horizontal sampling



Downward sampling



Upward sampling₇

Theory and method

- Sampling situations:

- Non-isokinetic

$$R = U_0 / U$$

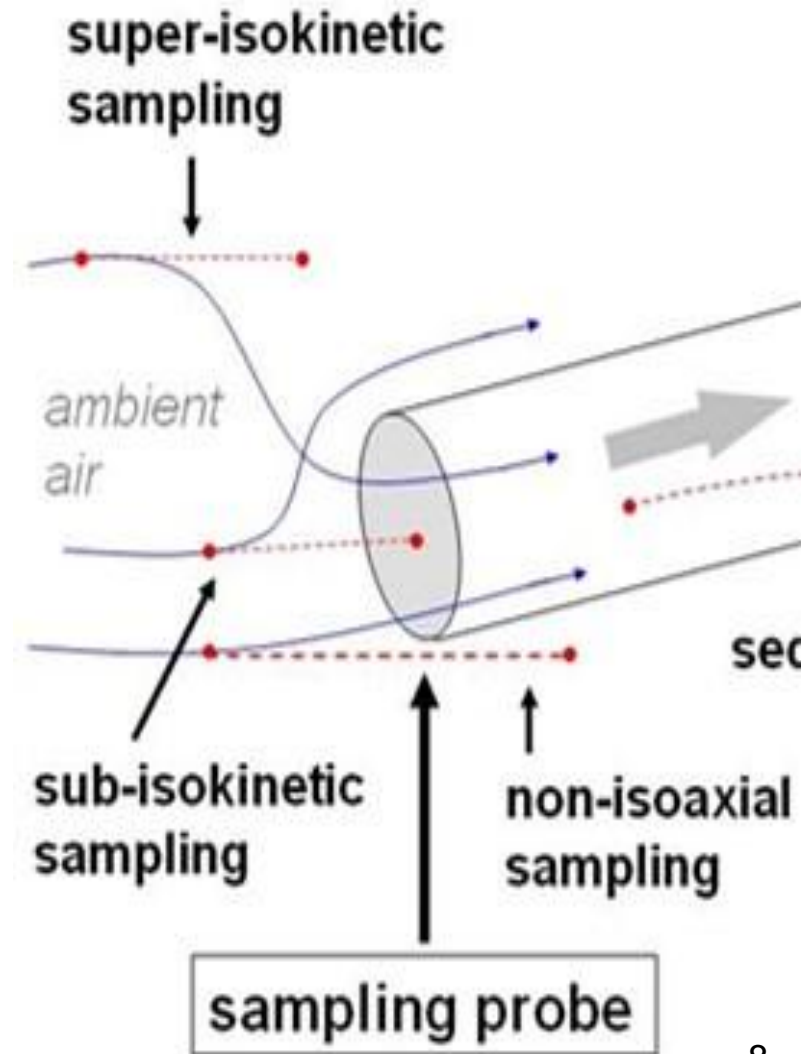
U_0 : local wind speed

U : flow velocity in the sampling probe

$R > 1$, sub-isokinetic sampling

$R < 1$, super-isokinetic sampling

- Isokinetic sampling ($R = 1$)



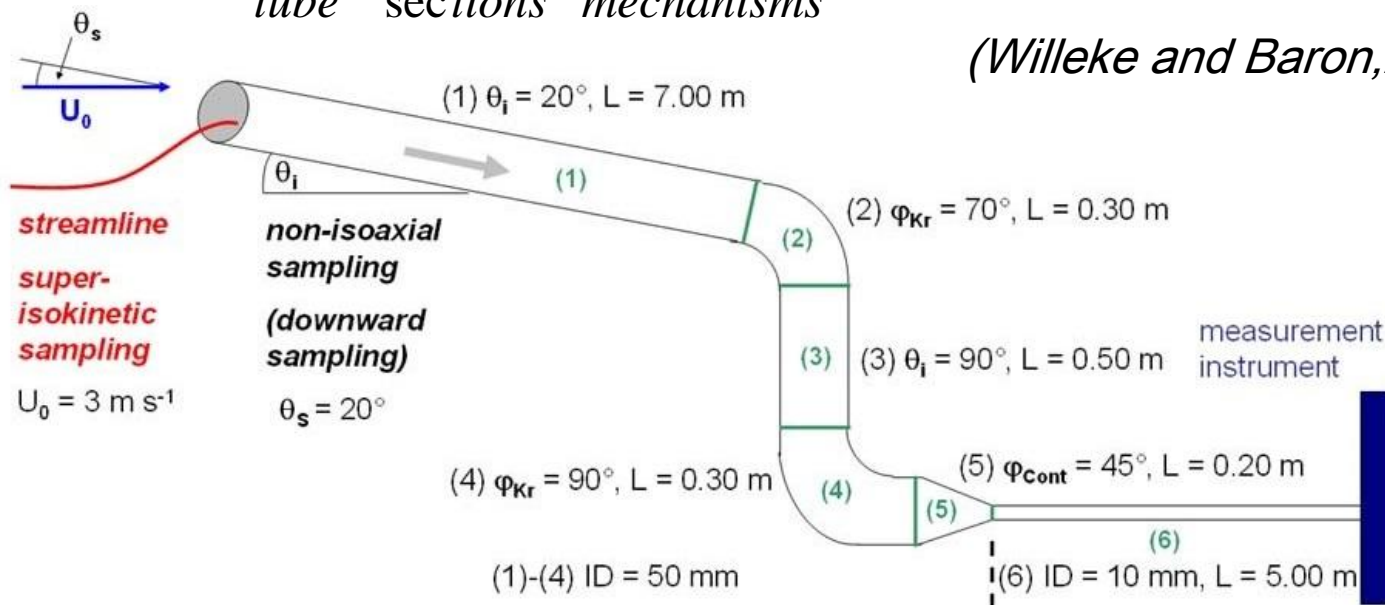
Theory and method

- Transport efficiency $\eta_{transport}$

The ratio of number concentration of aerosol particles leaving the transport tubing to that of those entering it.

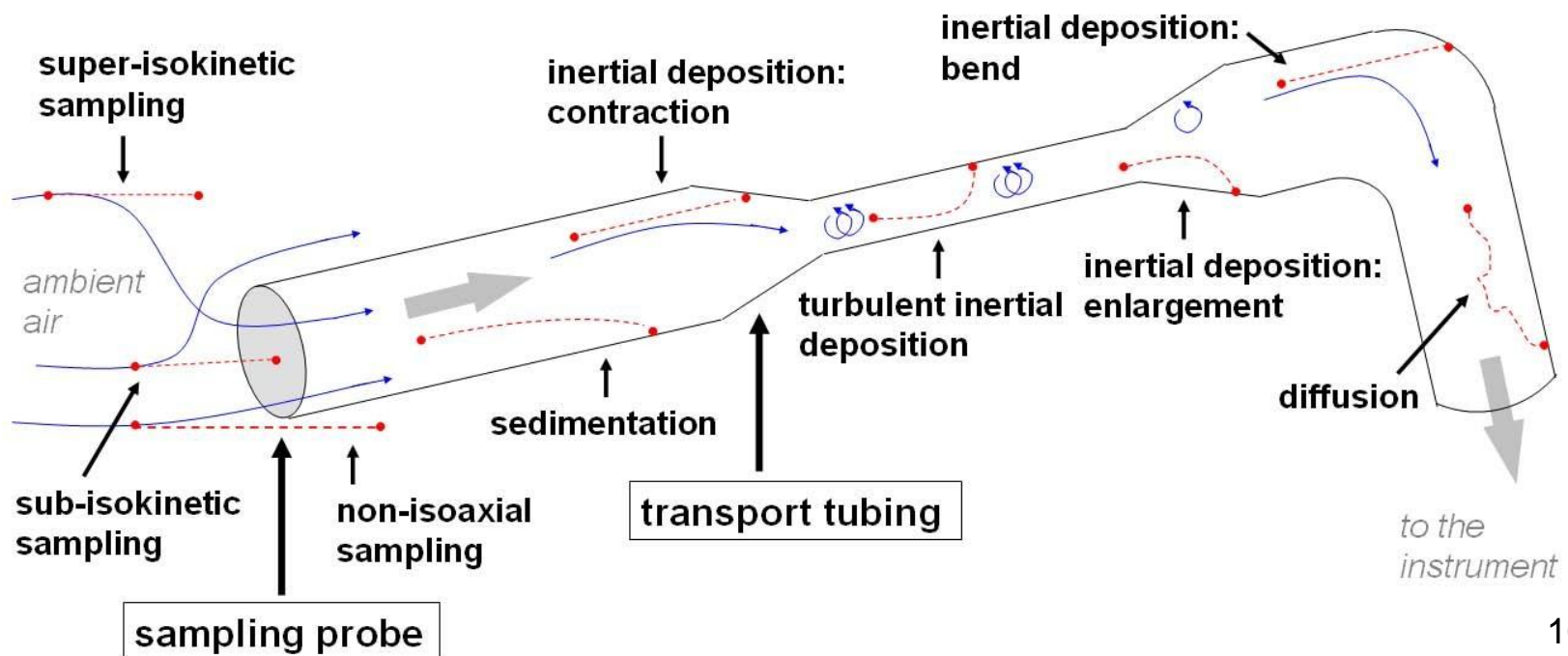
$$\eta_{transport}(d_a) = \prod_{tube} \left(\prod_{sections} \eta_{tube\ section, mechanism}(d_a) \right)$$

(Willeke and Baron, 2005)

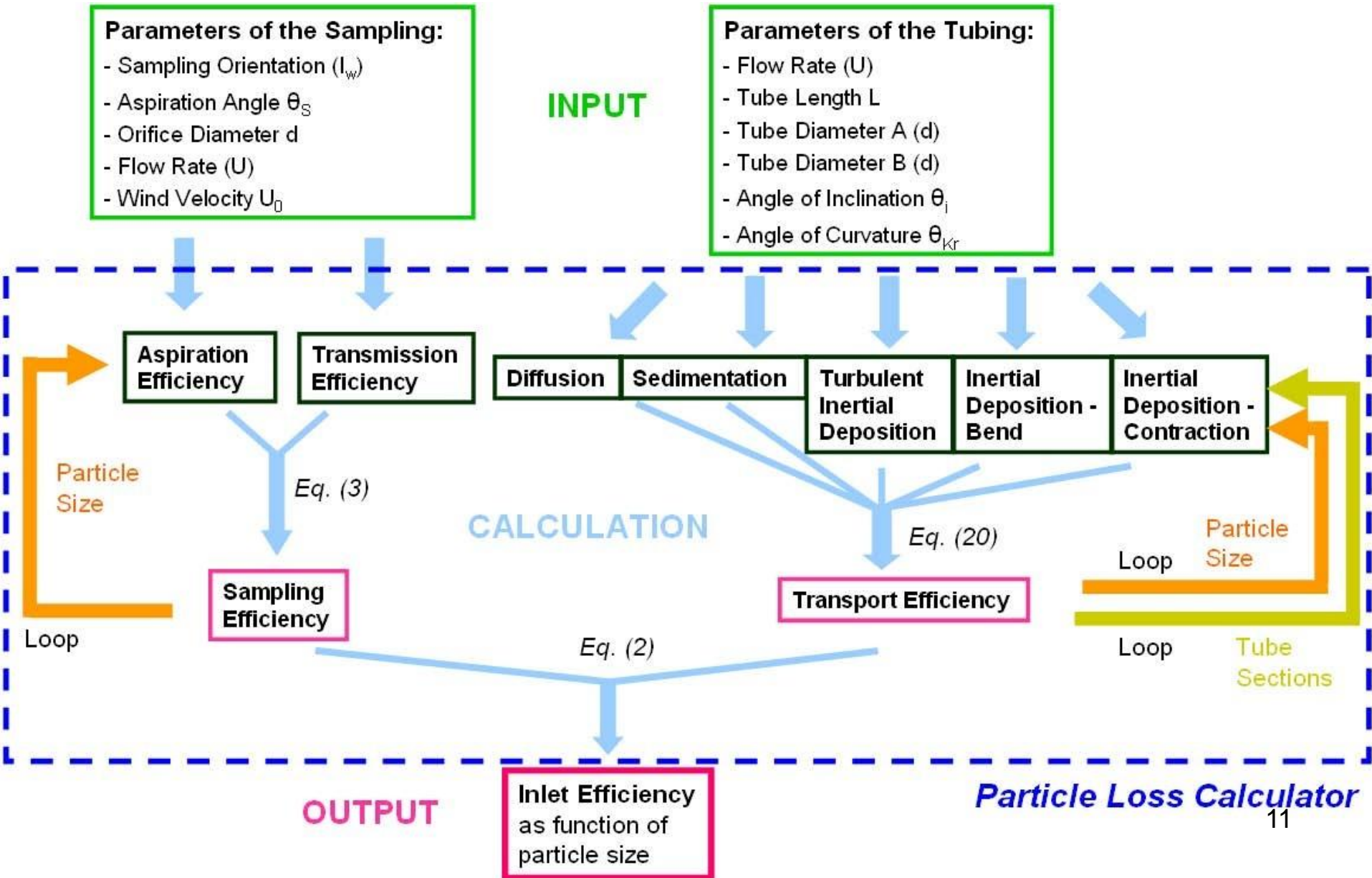


Theory and method

- Transport efficiency $\eta_{transport}$
- Diffusion efficiency η_{diff}
- Sedimentation η_{grav}
- Inertial deposition $\eta_{turb\ inert}$ $\eta_{bend,inert}$ $\eta_{cont,inert}$



Operation



Operation

Particle Loss Calculator

Max Planck Institute for Chemistry - Particle Chemistry Department
Sarah-Lena von der Weiden (2009)

Parameters of the Sampling:

☒ Account for Sampling Effects

Sampling Orientation: **Downward Sampling**

Aspiration Angle, °: **20**

Orifice Diameter, mm: **10**

Flow Rate, l/min: **10**

Wind Velocity, m/s: **3**

Aerosol Parameters:

Particle Density, kg/m³: **1000**

Shape Factor: **1**

Output Parameters:

Minimum Particle Size, µm: **0.01**

Maximum Particle Size, µm: **10**

Number of Size Points: **300**

Output: **Particle Loss (Whole Inlet)**

☒ Logarithmic Scale, X-Axis (dp)

☒ Logarithmic Scale, Y-Axis

Grid, X-Axis: **Major Only**

Grid, Y-Axis: **Major Only**

Parameters of the Tubing:

Number of Tube Sections: **7**

Edit Parameters **Load Parameters**

Save Parameters

Particle Loss Mechanisms:

☒ Diffusion ☒ Sedimentation

☒ Turbulent Inertial Deposition

☒ Inertial Deposition - Bend

☒ Inertial Deposition - Contraction

☒ Laminar Flow in Transition Regime

Help

Action!

Array of Curves:

☒ Array of Curves

Variable: **Tube Length**

from **1** steps **5**

to **10**

Operation

| Table0:No,flowrate,tubelength,... | | | | | | | |
|-----------------------------------|------------------|----------------|---------------------|---------------------|-------------------------|-----------------------|---|
| R8 | | | | 0 | | | |
| No | Flow Rate, l/min | Tube Length, m | Tube Diameter A, mm | Tube Diameter B, mm | Angle of Inclination, ° | Angle of Curvature, ° | |
| 1 | 4 | 0.05 | 10 | 10 | 0 | 0 | ^ |
| 2 | 4 | 0.1 | 10 | 20 | 45 | 0 | ≡ |
| 3 | 4 | 0.1 | 20 | 5 | 0 | 0 | |
| 4 | 1.2 | 0.083 | 5 | 10 | 0 | 0 | |
| 5 | 1.2 | 0.05 | 10 | 10 | 90 | 45 | |
| 6 | 1.2 | 0.033 | 10 | 3 | 90 | 0 | |
| 7 | 3 | 1.2 | 3 | 3 | 0 | 90 | v |

Validation

- Experimentally determined particle losses:

$$\text{particle loss}(\%) = \left(1 - \frac{\text{number conc. of particles at tube exit}}{\text{number conc. of particles at tube entrance}}\right) \cdot 100\%$$

- Experiment instrument:

| instrument | size range | correction factor |
|---|------------|-------------------|
| Condensation Particle Counter (CPC,TSI,model 3007) | 10nm-250nm | 1.0094 |
| Optical Particle Counter (OPC,Trimm,model 1.109) | 300nm-32μm | concerning size |

Table 1. Correction factor applied to one of the OPCs during the outdoor validation measurements

| Particle Size (μm) | | | | | | | | |
|--------------------|--------|--------|--------|--------|--------|-------|--------|--------|
| | 0.265 | 0.290 | 0.325 | 0.375 | 0.425 | 0.475 | 0.54 | 0.615 |
| | 0.675 | 0.750 | 0.900 | 1.150 | 1.450 | 1.800 | 2.250 | 2.750 |
| | 3.250 | 4.500 | 5.750 | 7.000 | 8.000 | 9.250 | 11.250 | 13.750 |
| | 16.250 | 18.750 | 22.500 | 27.500 | 31.000 | | | |
| Correction Factor | | | | | | | | |
| | 0.841 | 0.998 | 1.015 | 0.968 | 0.840 | 0.609 | 1.028 | 0.870 |
| | 0.920 | 1.101 | 0.816 | 1.125 | 0.930 | 0.903 | 0.963 | 0.925 |
| | 0.881 | 0.912 | 0.833 | 0.985 | 0.868 | 1 | 1 | 1 |
| | 1 | 1 | 1 | 1 | 1 | | | |

Validation

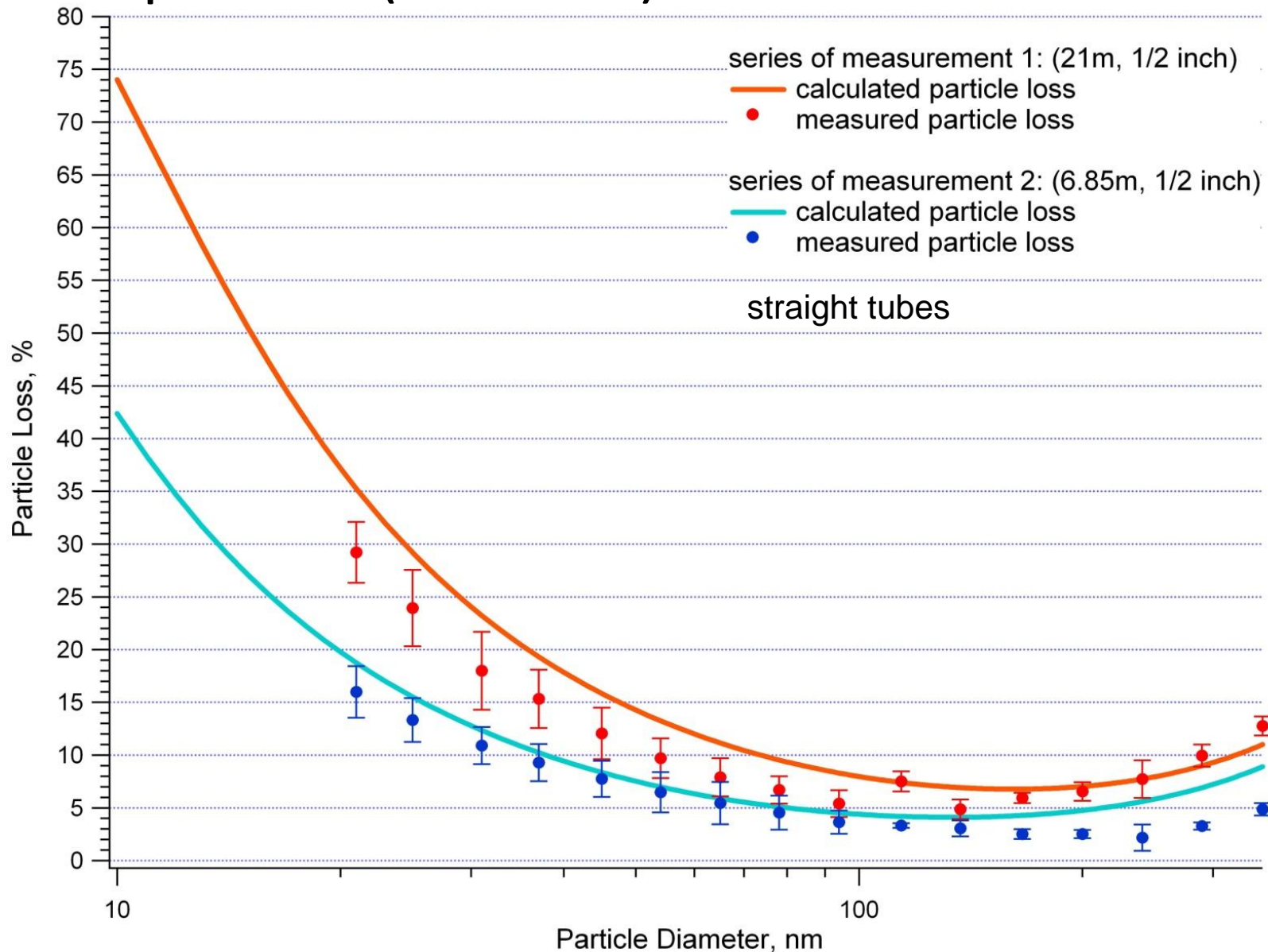
- Small particles (diffusion)
- Devices:

| | |
|----------|-----------------------------------|
| ID | 1/4 inch |
| lengths | 20.80m,10m,3m |
| geometry | coiled in several turns(up to 10) |

- Results:
 - a. There're similar trends between particle the losses measured and those calculated.
 - b. There're differences in the size range from about 20nm to 200nm,which depend on the angle of curvature.
 - c. Particle loss due to inertial effects is not negligible for small particles in a laminar flow in the range tested.

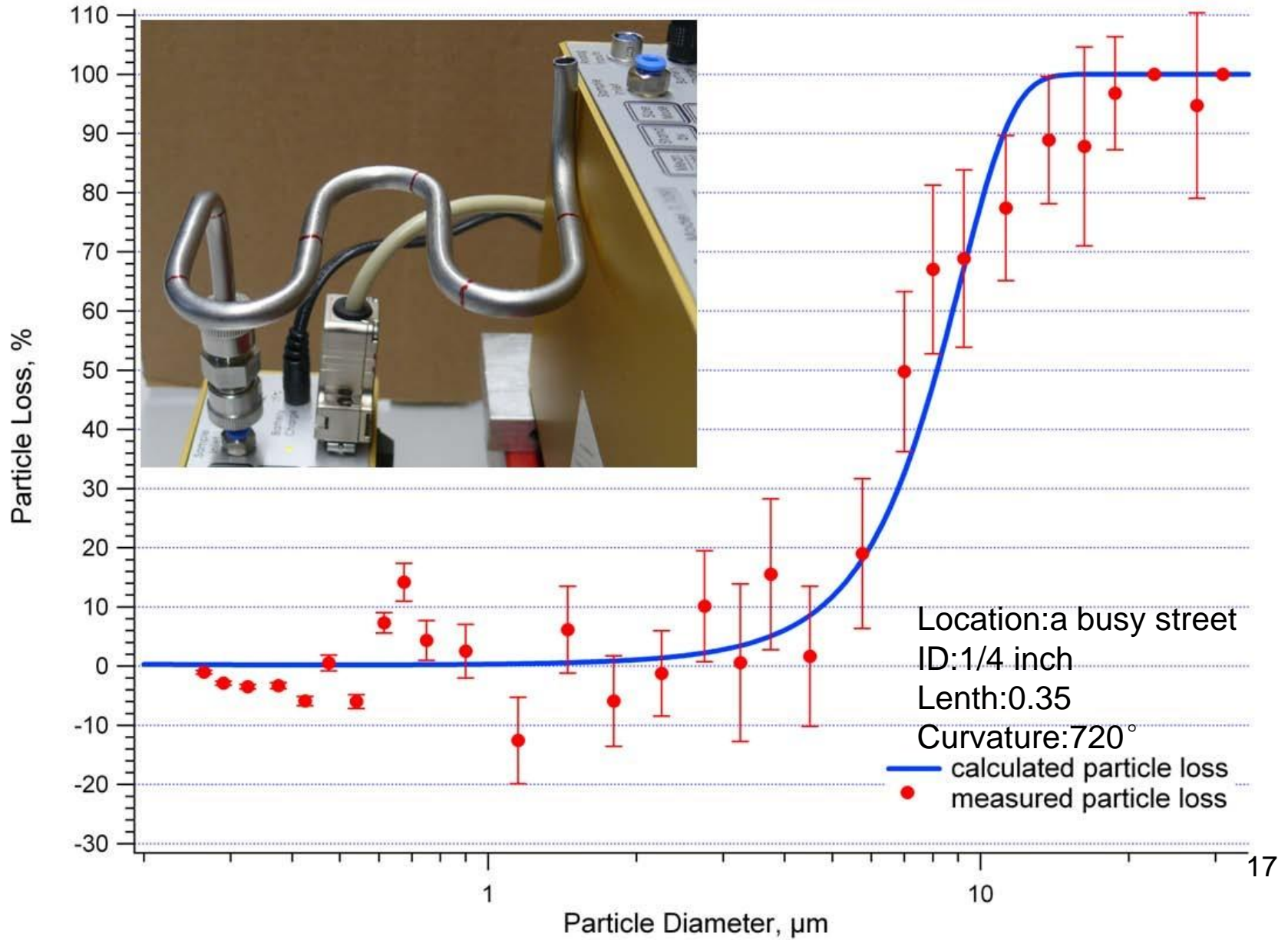
Validation

● Small particles(diffusion)

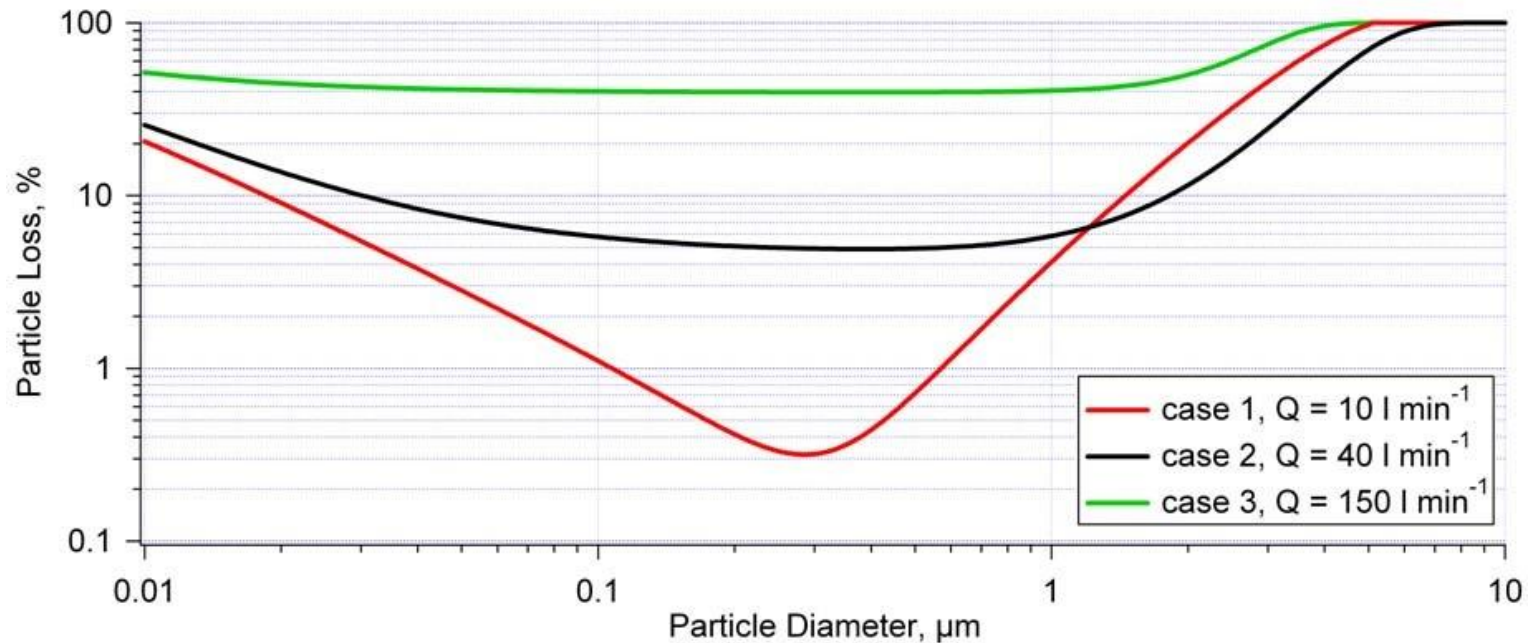
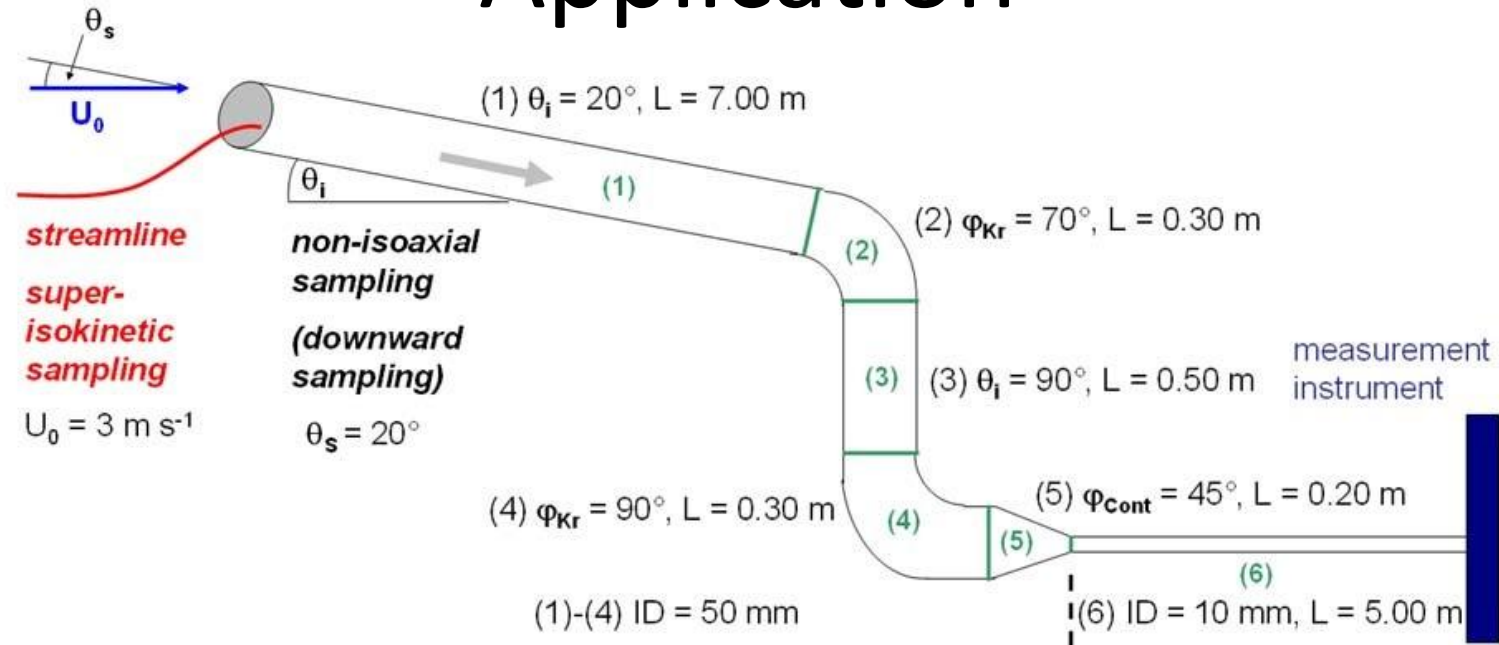


Validation

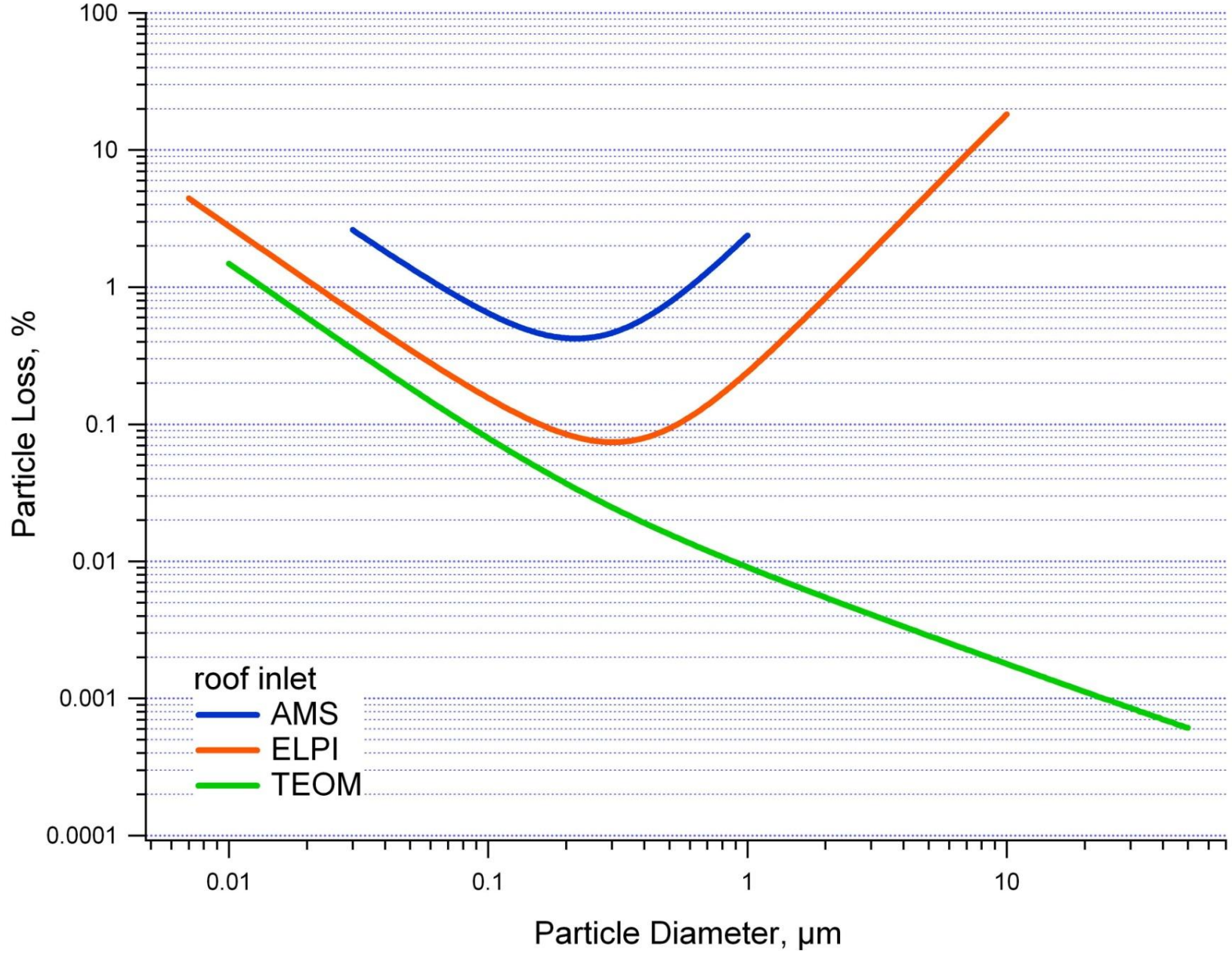
- Larger particles (impaction losses in bends)



Application



Application



Summary

- Calculations from PLC agree well with those from experiment for less extreme geometries.
- The software PLC based on both empirically and theoretically derived relations can quickly assess aerosol sampling efficiencies and particle transport losses for arbitrary tubing system.

THANK YOU